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ADVANCES IN HYDRAULIC RESEARCH



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**Development of a generalized criterion for selecting optimal MRF rotation zone for CFD simulation of stirred tank reactors**

By

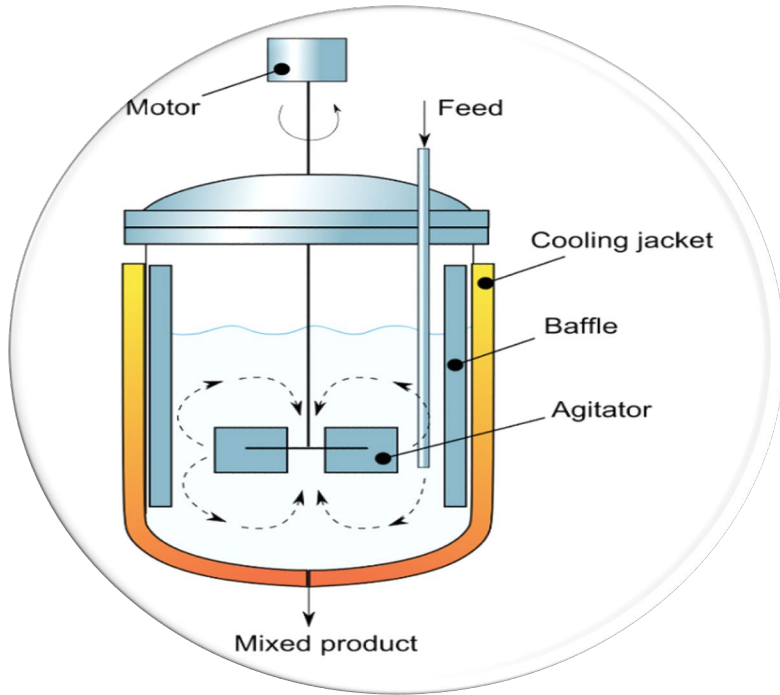
Devarajan Krishna Iyer<sup>1</sup> and Ajey Kumar Patel<sup>2</sup>

Ph.D. Scholar<sup>1</sup> and Associate Professor<sup>2</sup>, NIT Warangal,  
Warangal, Telangana, India

# OUTLINE OF PRESENTATION

- ❖ Introduction
- ❖ MRF approach
- ❖ MRF boundary
- ❖ Stirred tank configuration
- ❖ Computational Methodology
- ❖ Governing equations
- ❖ Computational grid
- ❖ Convergence of CFD simulation
- ❖ Grid independence study
- ❖ Position of MRF boundary
- ❖ Conclusions
- ❖ Acknowledgements
- ❖ References

# INTRODUCTION



**Mixing,  
Blending**

- **Chemical processes**
- **Reactive flows**

**Solid-liquid  
suspension**

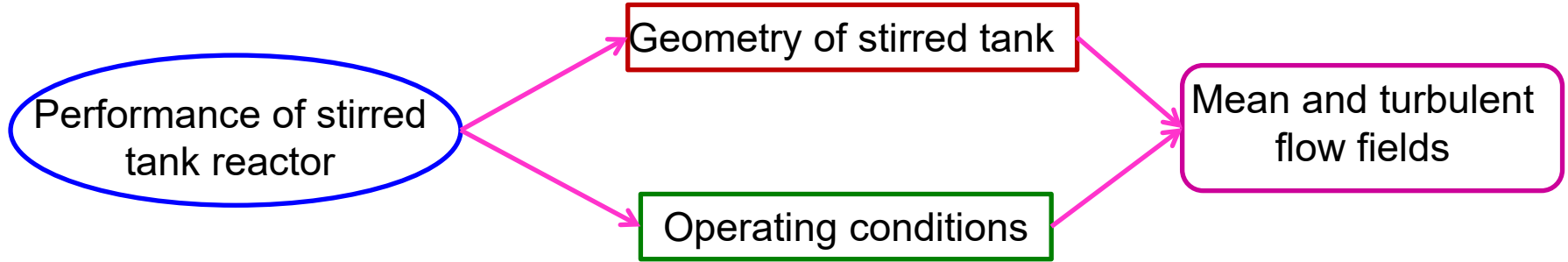
- **Pump-mix mixers**
- **Dissolution**
- **Ion exchange**

**Dispersion,  
Contacting**

- **Surface aeration**
- **Animal Cell cultures**

Fig. 1: Stirred tank reactor and its applications (Source: <https://www.comsol.com>)

# INTRODUCTION Contd.



- Proper **design** requires detailed knowledge of **stirred tank hydrodynamics**
- **Computational Fluid Dynamics** (CFD) → Popular tool for predicting tank hydrodynamics
- Modelling of **impeller rotation** is a major challenge
- **Multiple Reference Frame (MRF) approach** → Popular model for impeller rotation

# MRF APPROACH

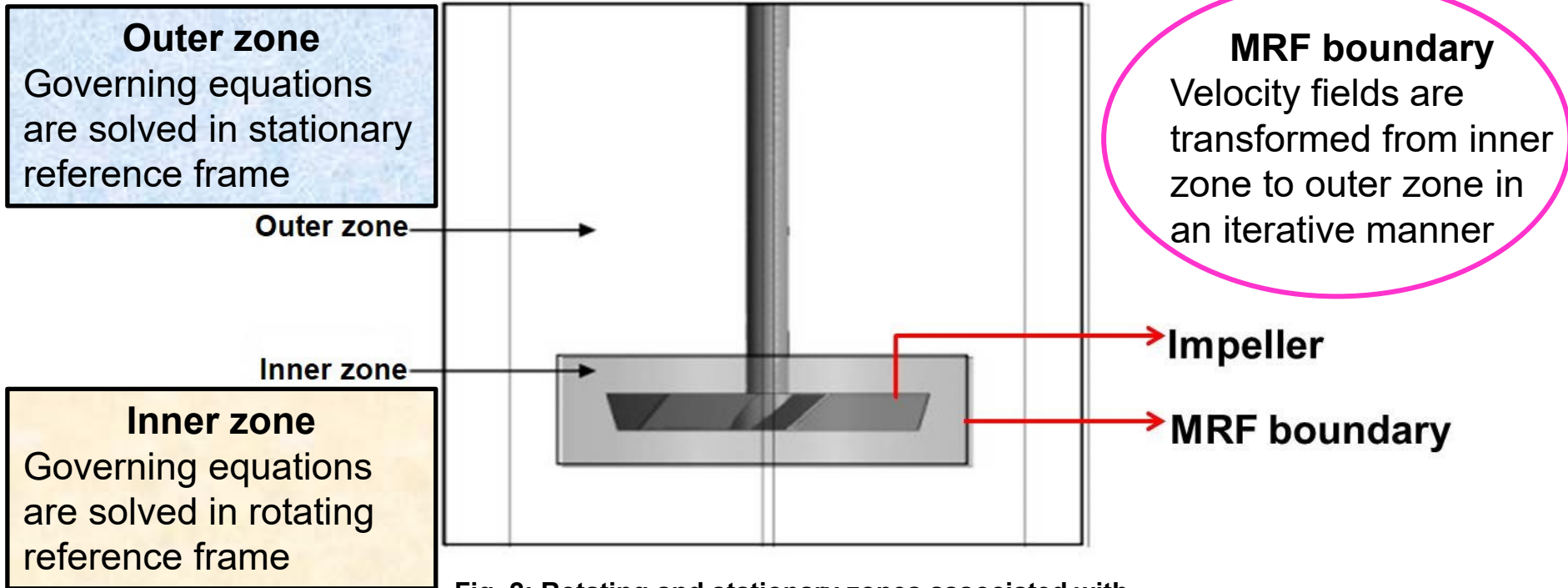
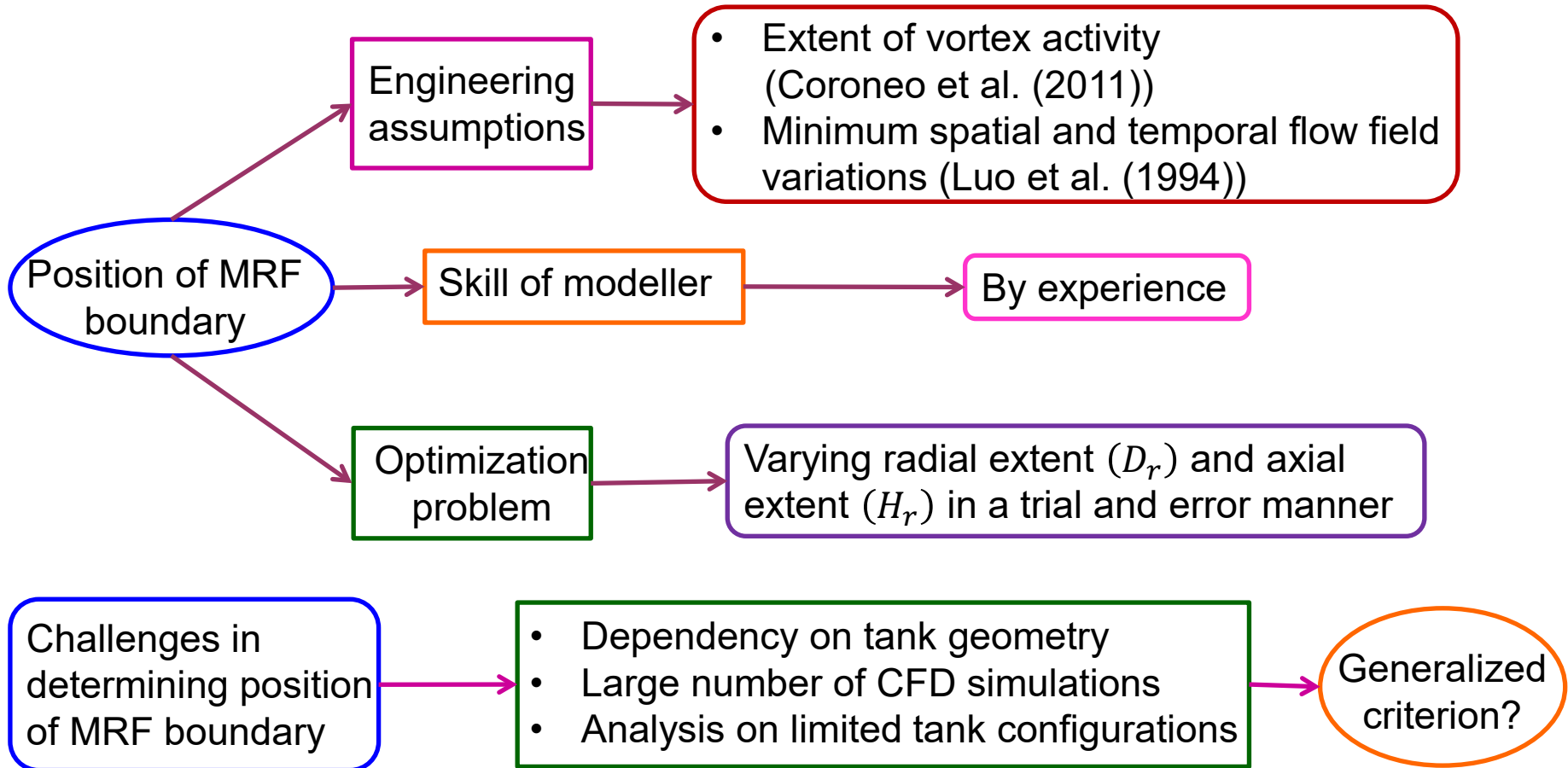


Fig. 2: Rotating and stationary zones associated with the stirred tank reactor (Source: Joshi et al. (2011))

- ✓ Improper position of MRF boundary increases round-off errors and decreases accuracy and numerical convergence of simulations

# MRF BOUNDARY



# MRF BOUNDARY Contd.

Authors	Optimal MRF boundary	Remarks
Oshinowo et al. (2000)	$D_r : 2.05D$ $H_r : \pm 0.5D$	Optimal axial extent was determined while radial extent was kept constant
Zadravec et al. (2007)	$D_r : 1.43D$ $H_r : 0.63D$	Larger extents of MRF boundary are suitable for modelling reactor vessels
Shi and Rzehak (2017)	$D_r : 1.66D$ $H_r : \pm 1.452D$	Optimal radial extent was determined while axial extent was kept constant
Patil et al. (2021)	$D_r : 2D$ $H_r : 0.62D$	Optimal extents were determined from mean velocity predictions
Mittal and Kikugawa (2021)	$D_r : 1.4D$ $H_r : 0.42D$	MRF boundary near impeller or baffle walls generate unsteady effects in tank

- ✓ **Objective:** Development of a **generalized criterion** for determining optimal extents of MRF boundary for **any configuration of stirred tank reactor**

# STIRRED TANK CONFIGURATION

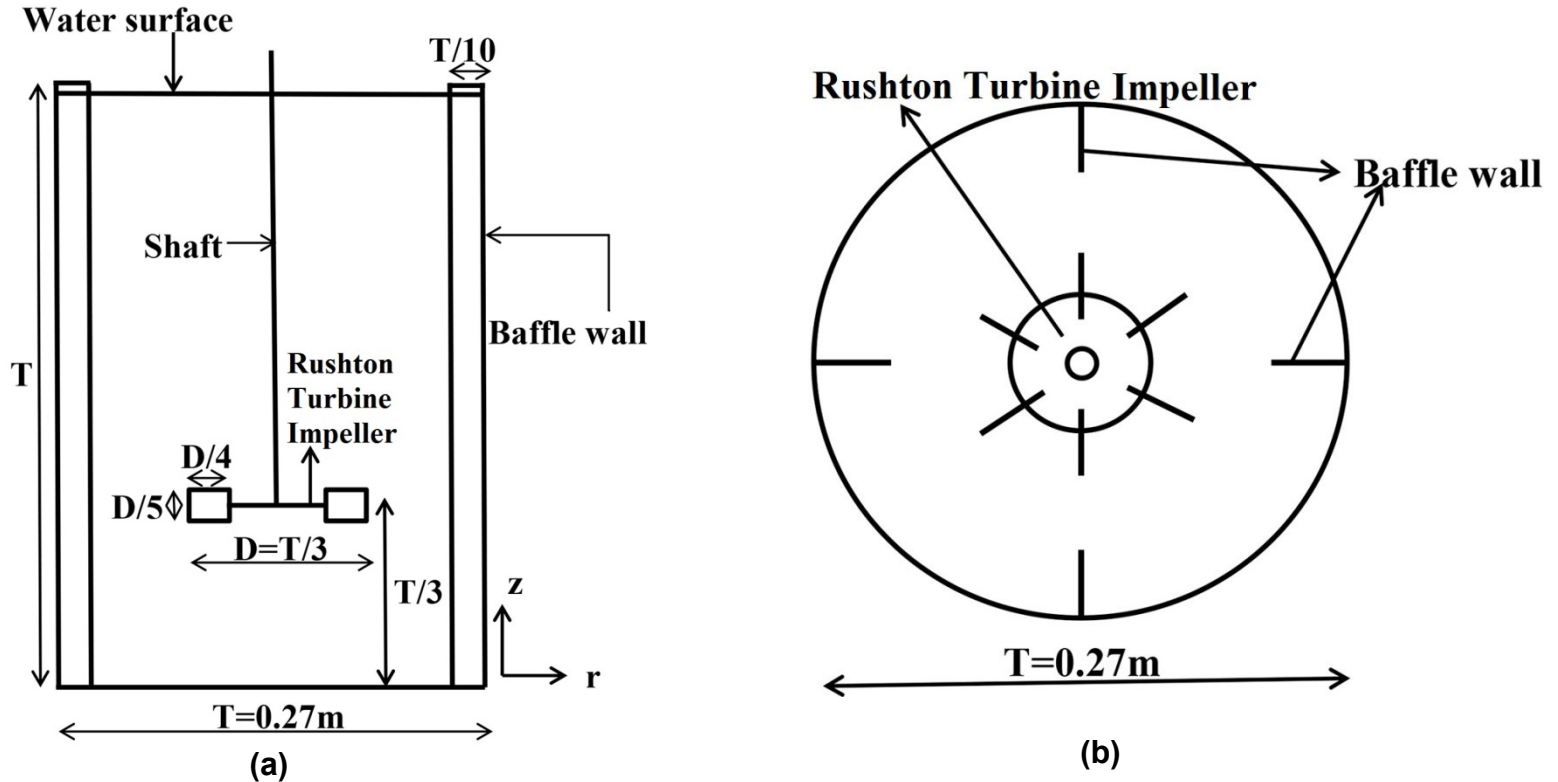


Fig. 3: (a) Sectional elevation and (b) Plan of the standard configuration of stirred tank reactor adopted for the present study (Impeller speed: 200 rpm; Reynolds number: 29,000) (Source: Wu and Patterson (1989))



# COMPUTATIONAL METHODOLOGY

Parameter	Approach adopted for CFD simulations
Modelling approach	Steady state three dimensional Reynolds Averaged Navier Stokes (RANS) equations
Turbulence model	Standard $k - \varepsilon$ turbulence model
Impeller rotation model	Multiple Reference Frame (MRF) impeller modelling scheme
Boundary conditions	Tank periphery, tank bottom, impeller: No-slip boundary condition Tank top surface: Symmetry boundary condition
Pressure-Velocity coupling scheme	SIMPLE scheme
Discretization scheme	Second order upwind scheme
Convergence criteria	$10^{-6}$
Workstation	Double precision 64 bit Intel (R) Xeon (R) E5-1620 3.6 GHz processor with 12 cores
Software	ANSYS 17.0 version

# GOVERNING EQUATIONS

Continuity equation:

$$\nabla \cdot (\rho \vec{\mathbf{u}}) = 0 \quad (1)$$

Momentum equation:

$$\nabla \cdot (\rho \vec{\mathbf{u}} \vec{\mathbf{u}}) = -\nabla P + \nabla \cdot (\vec{\tau} + \overline{\tau^R}) + \rho \vec{g} + \overline{F^{MRF}} \quad (2)$$

Turbulent viscosity ( $\mu_t$ ) from standard  $k - \varepsilon$  model:

$$\mu_t = C_\mu \rho \frac{k^2}{\varepsilon} \quad (3)$$

Transport equations of  $k$  and  $\varepsilon$ :

$$\nabla \cdot (\rho \vec{\mathbf{u}} k) = \nabla \cdot \left( \frac{\mu_t}{\sigma_k} \nabla k \right) + G_k - \rho \varepsilon \quad (4)$$

$$\nabla \cdot (\rho \vec{\mathbf{u}} \varepsilon) = \nabla \cdot \left( \frac{\mu_t}{\sigma_\varepsilon} \nabla \varepsilon \right) + \frac{\varepsilon}{k} (C_{1\varepsilon} G_k - C_{2\varepsilon} \rho \varepsilon) \quad (5)$$

# GOVERNING EQUATIONS Contd.

## Performance goals

Power number based on impeller torque ( $N_{pt}$ ): 
$$N_{pt} = \frac{2\pi N\tau}{\rho N^3 D^5} \quad (6)$$

Power number based on turbulence dissipation rate ( $N_{p\varepsilon}$ ): 
$$N_{p\varepsilon} = \frac{\iiint \rho \varepsilon dV}{\rho N^3 D^5} \quad (7)$$

Energy imbalance = 
$$\frac{N_{pt} - N_{p\varepsilon}}{N_{pt}} \quad (8)$$

## Terminology

$\rho$ : Time averaged density

$P$ : Static pressure

$\mathbf{u}$ : velocity of fluid

$\bar{\tau}$ : Viscous stress tensor

$\overline{\tau^R}$ : Reynolds stress tensor

$\rho \vec{g}$ : Gravitational body force

$\overrightarrow{F^{MRF}}$ : Centrifugal and coriolis forces

$k$ : Turbulent kinetic energy

$\varepsilon$ : Turbulent dissipation rate

$G_k$ : Turbulence generation rate

$\sigma_k, \sigma_\varepsilon$ : Turbulent Prandtl numbers

$C_{1\varepsilon}, C_{2\varepsilon}$ : constants

$C_\mu = 0.09, C_{1\varepsilon} = 1.44, C_{2\varepsilon} = 1.92$

$\sigma_k = 1, \sigma_\varepsilon = 1.3$

$\tau$ : Net impeller torque

$D$ : Diameter of impeller

$N$ : Impeller speed

# COMPUTATIONAL GRID

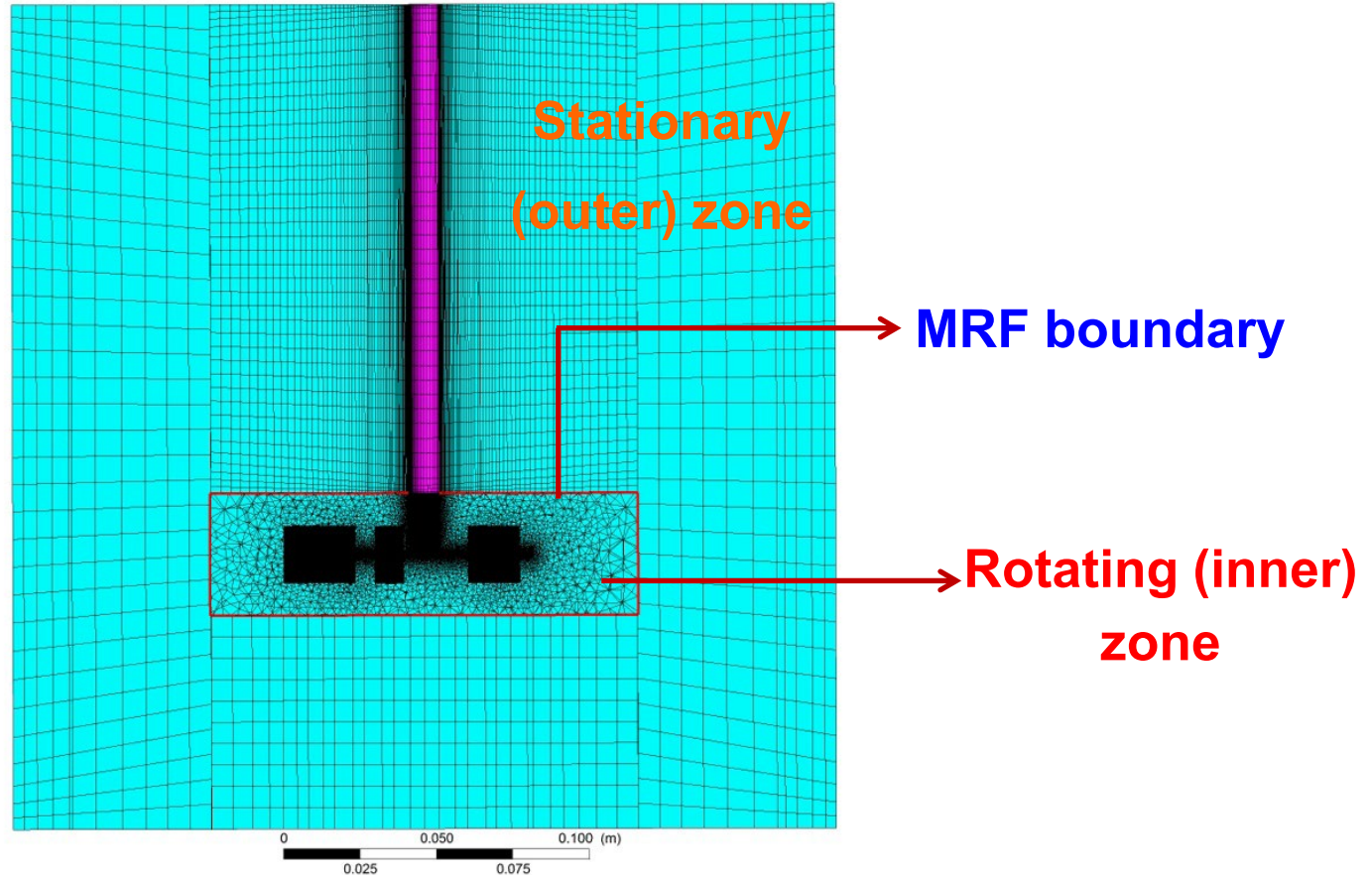


Fig. 4: Computational grid (Hybrid grid type) developed for the present study

# CONVERGENCE OF CFD SIMULATION

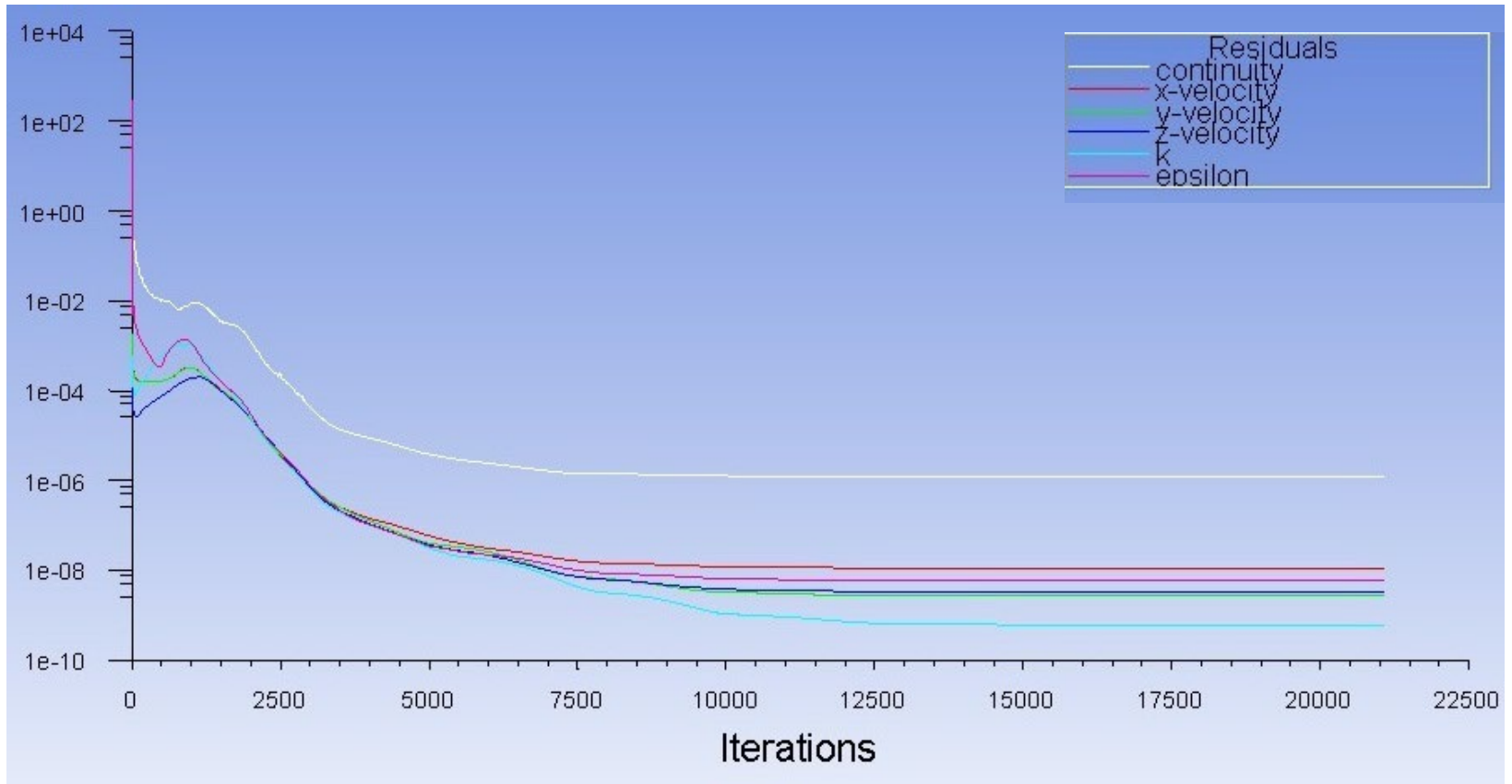


Fig. 5: Typical convergence curve from the CFD model with optimal MRF boundary

# GRID INDEPENDENCE STUDY

- Grid independence study was performed for all computational trials
- Size of tetrahedral elements comprising the impeller was successively reduced
- Normalized radial velocity  $\left(\frac{u_r}{u_{tip}}\right)$  was monitored for assessing the grid convergence of the CFD model

**Table 1: Details of grids used for the grid independence study ( $D_r \times H_r$  of 14 cm×4 cm)**

Grid	Element size of impeller (m)	Number of elements
Grid-1	0.004	300573
Grid-2	0.0008	996072
Grid-3	0.00035	4497937
Grid-4	0.000258	7418360
Grid-5	0.00024	8451837

# GRID INDEPENDENCE STUDY Contd.

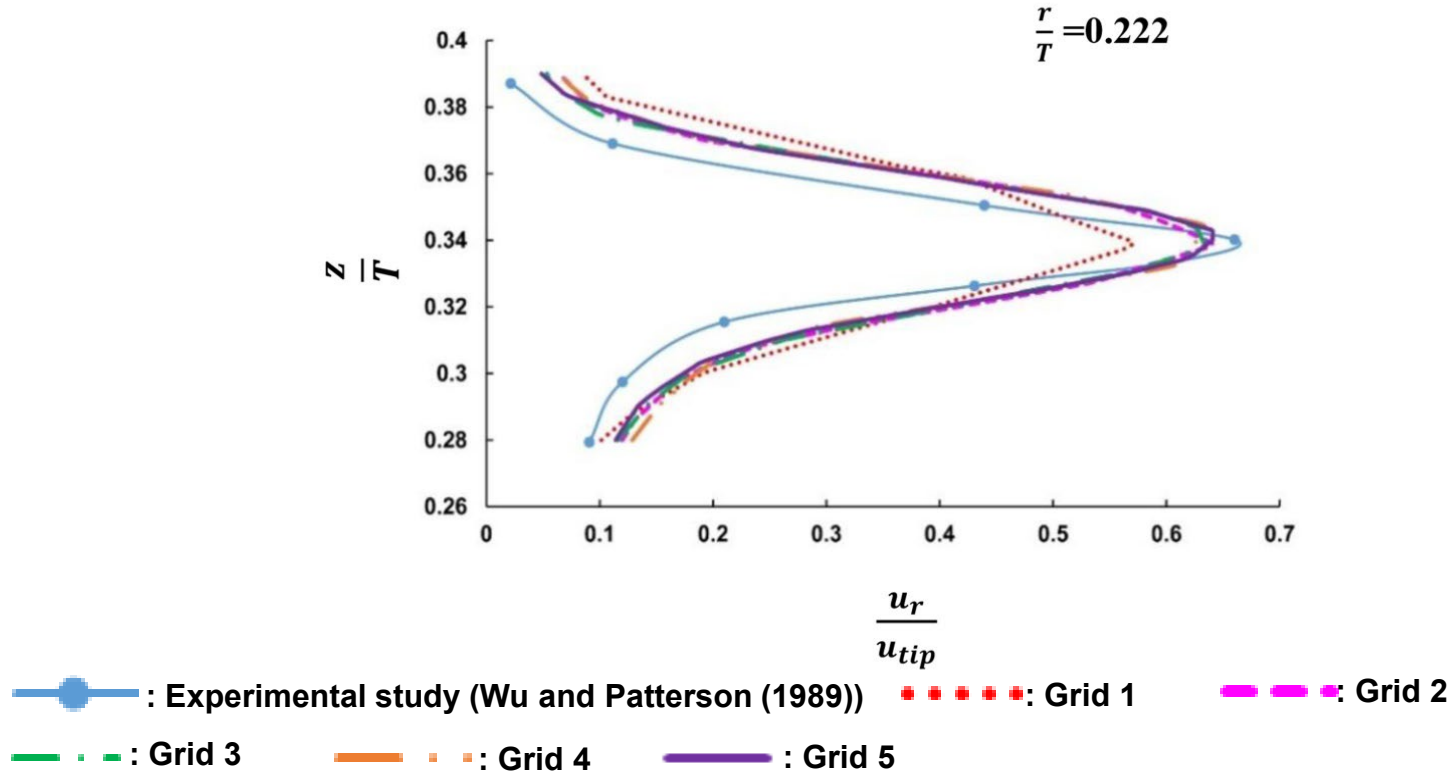


Fig. 6: Variation of axial profile of  $\frac{u_r}{u_{tip}}$  close to the impeller with grid resolution

# GRID INDEPENDENCE STUDY Contd.

- **Verification** process:
  - $\frac{u_r}{u_{tip}}$  increases from Grid-1 to Grid-3 and becomes constant thereafter
  - Predictions from Grid-4 were found to be independent of grid resolution
  - Grid convergence Index of peak  $\frac{u_r}{u_{tip}}$  is only 1.27%
- **Validation** process:
  - Accurate prediction of magnitude and location of peak  $\frac{u_r}{u_{tip}}$
  - Predictions of  $\frac{u_r}{u_{tip}}$  from Grid-4 are in excellent agreement with experimental results of Wu and Patterson (1989)
  - Present CFD model accurately predicts flow behaviour of standard stirred tank reactor



# POSITION OF MRF BOUNDARY

- $\frac{D_r}{D}$  and  $\frac{H_r}{D}$  were varied from near impeller region to the periphery of the stirred tank
- Effect of  $\frac{D_r}{D}$  and  $\frac{H_r}{D}$  on  $N_{pt}$  and  $N_{p\varepsilon}$  were analysed
- Optimal  $\frac{D_r}{D}$  and  $\frac{H_r}{D}$  were selected by comparing the predictions of  $N_{pt}$  and  $N_{p\varepsilon}$  with experimental results

**Table 2: Upper and lower limits of  $D_r$  and  $H_r$  adopted for the computational trials**

MRF boundary extent	General limits for any geometry	Possible limits for the present study
$D_r$	$D < D_r < (T - 2B)$	9.3 cm $< D_r <$ 21.6 cm
$H_r$	$h < H_r < 2h$	1.86 cm $< H_r <$ 18 cm

Where  $B = \frac{T}{10}$ ,  $h = \frac{T}{3}$

# POSITION OF MRF BOUNDARY Contd.

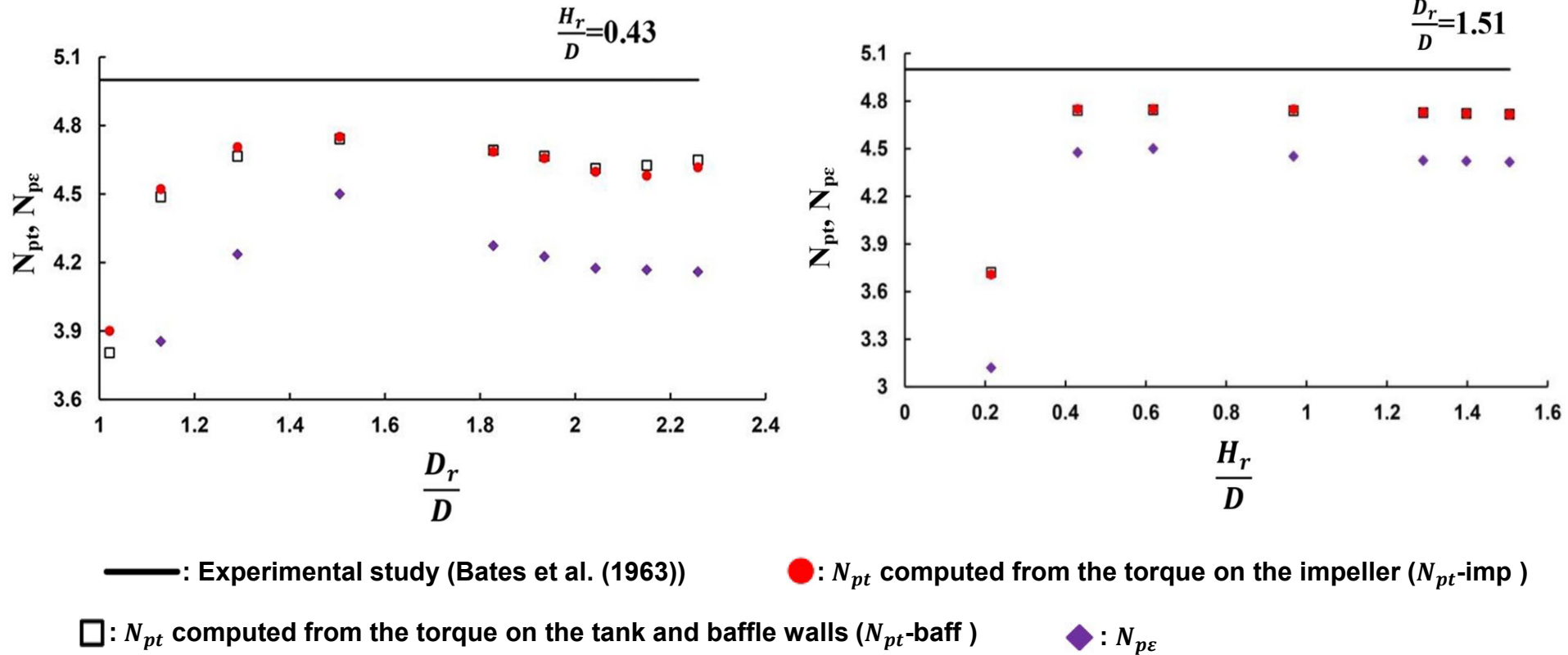


Fig. 7: Variation of  $N_{pt}$  and  $N_{p\epsilon}$  with (a)  $\frac{D_r}{D}$  and (b)  $\frac{H_r}{D}$

# POSITION OF MRF BOUNDARY Contd.

❑ Medium  $\frac{D_r}{D}$  (1.51-1.94) and larger  $\frac{H_r}{D}$  ( $>\pm 0.22$ ):

- ❖ Provides superior matching between  $N_{pt}$ -imp and  $N_{pt}$ -baff
- ❖ Proper transfer of impeller power towards tank periphery
- ❖ Produces accurate prediction of  $N_{p\varepsilon}$
- ❖ Optimal MRF boundary

❑ Smaller  $\frac{D_r}{D}$  (1.05-1.29), smaller  $\frac{H_r}{D}$  (0.22) and larger  $\frac{D_r}{D}$  (2.04-2.26):

- ❖ Provides inadequate matching between  $N_{pt}$ -imp and  $N_{pt}$ -baff
- ❖ Improper transfer of impeller power towards tank periphery
- ❖ Inaccurate predictions of  $N_{p\varepsilon}$

❑ Higher sensitivity of  $\frac{D_r}{D}$  as compared to  $\frac{H_r}{D}$

# POSITION OF MRF BOUNDARY Contd.

- ❑ Medium  $\frac{D_r}{D}$  and larger  $\frac{H_r}{D}$  exist at **suitable distance** from the impeller which results in **proper transformation of velocity fields at MRF boundary** and **accurate prediction** of various flow field quantities
- ❑ **Generalized criterion for selecting optimal MRF boundary:**
  - ❖ **Proper balance between  $N_{pt}$ -imp and  $N_{pt}$ -baff**
  - ❖ Based on **principle of conservation of angular momentum**
  - ❖ Applied to **any configuration of stirred tank reactor**
- ❑ Optimal range of MRF extents from this study includes the MRF extents provided by Patil et al. (2021) and Zadavec et al. (2007)

# POSITION OF MRF BOUNDARY Contd.

Table 3: Comparison of errors related with  $N_{pt}$  and  $N_{p\varepsilon}$  from the present study and that from other literature

Authors	Turbulence model	Error related with $N_{pt}$ (%)	Error related with $N_{p\varepsilon}$ (%)	Energy imbalance
Singh et al. (2011)	Standard $k - \varepsilon$ model	14.00	2.00	10.53
	SAS-SST	38.00	4.00	24.64
	SSG-RSM	30.00	10.00	15.38
	SST-CC	32.00	10.00	31.82
Murthy and Joshi (2008)	Standard $k - \varepsilon$ model	3.92	23.53	20.41
	RSM	1.96	19.61	18.00
	LES	1.96	7.84	9.62
<b>Present study</b>	<b>Standard <math>k - \varepsilon</math> model</b>	<b>5.00</b>	<b>10.00</b>	<b>5.26</b>

- ✓ CFD model with **optimal MRF boundary** significantly improves the **predictive capability of standard  $k - \varepsilon$  turbulence model**

# CONCLUSIONS

- A **generalized criterion** for determining the **optimal position of MRF boundary** was developed
- $\frac{D_r}{D}$  and  $\frac{H_r}{D}$  were varied in the entire domain of stirred tank reactor
- $\frac{D_r}{D}$  and  $\frac{H_r}{D}$  **close to the impeller and tank periphery** were found to be **unsuitable** for modelling the stirred tank reactors
- **Medium**  $\frac{D_r}{D}$  and **larger**  $\frac{H_r}{D}$  were found to be **appropriate for modelling** the stirred tank reactors
- **Balance between  $N_{pt-imp}$  and  $N_{pt-baff}$**  was determined as the generalized criterion
- CFD model with optimal MRF boundary significantly improves the predictive capability of standard  $k - \varepsilon$  turbulence model

# ACKNOWLEDGEMENTS

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